

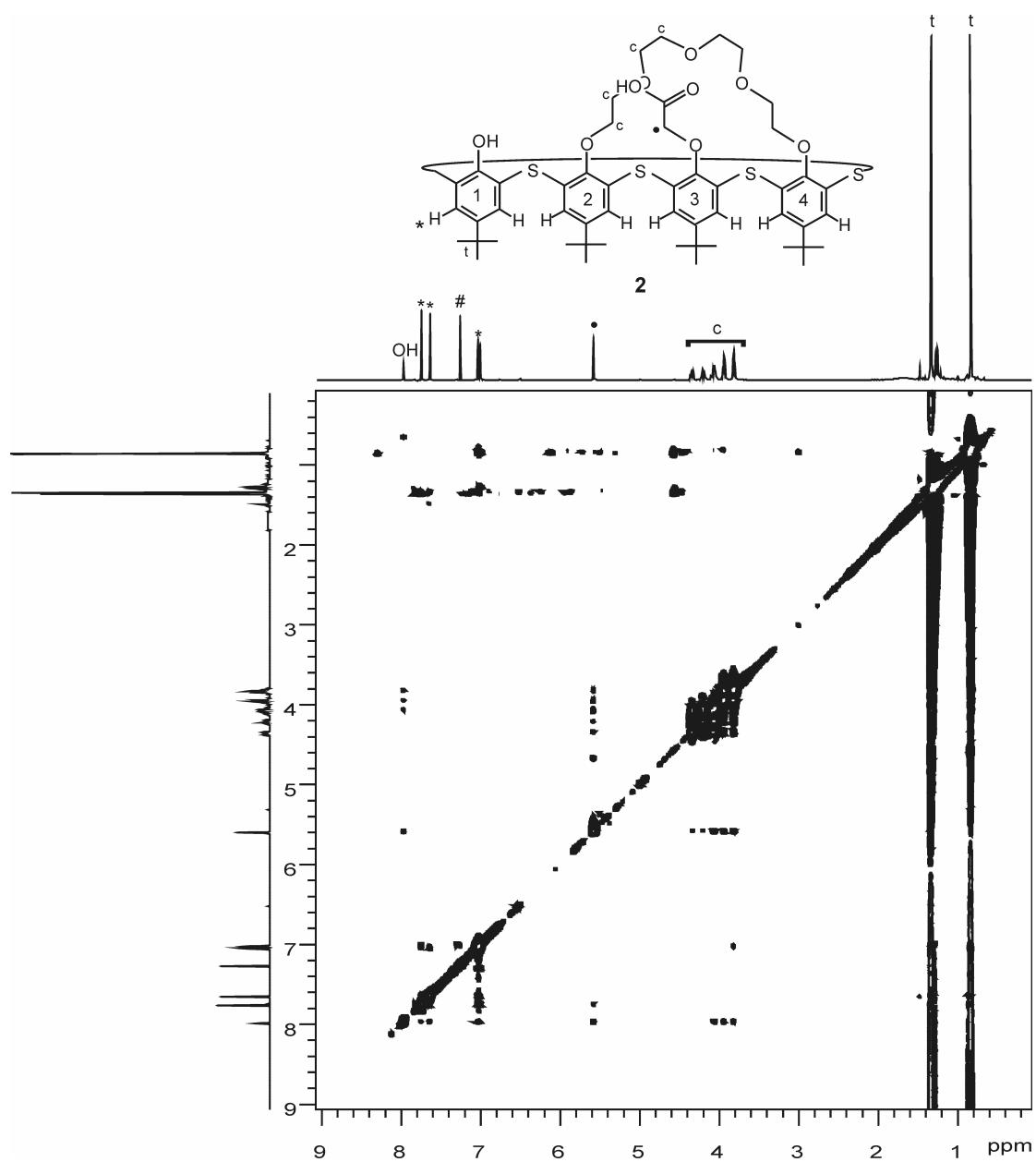
**Electronic supplementary information**

**Thiacalix[4]arene derivatives as radium ionophores: a study on the requirements for  $^{226}\text{Ra}^{2+}$  extraction**

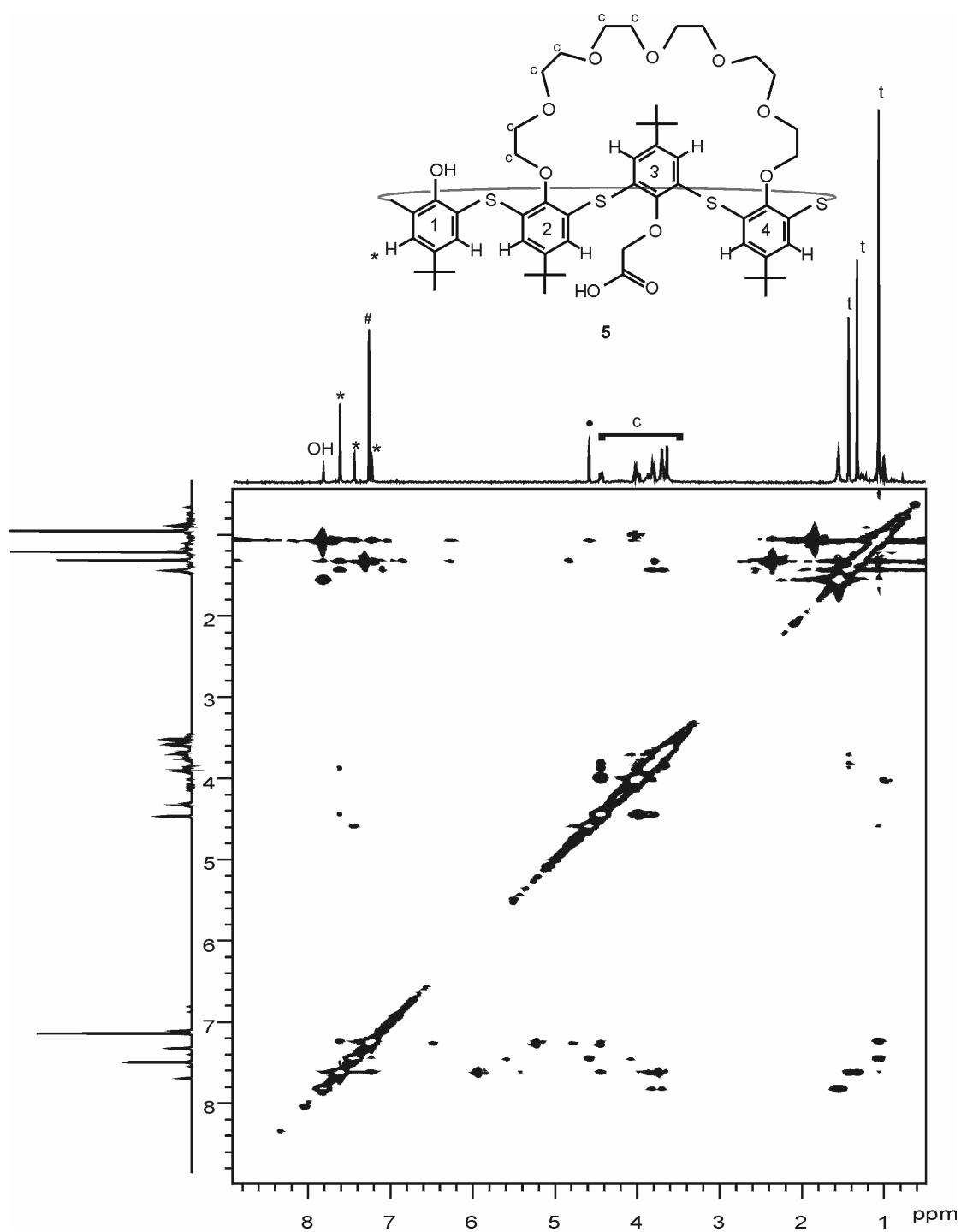
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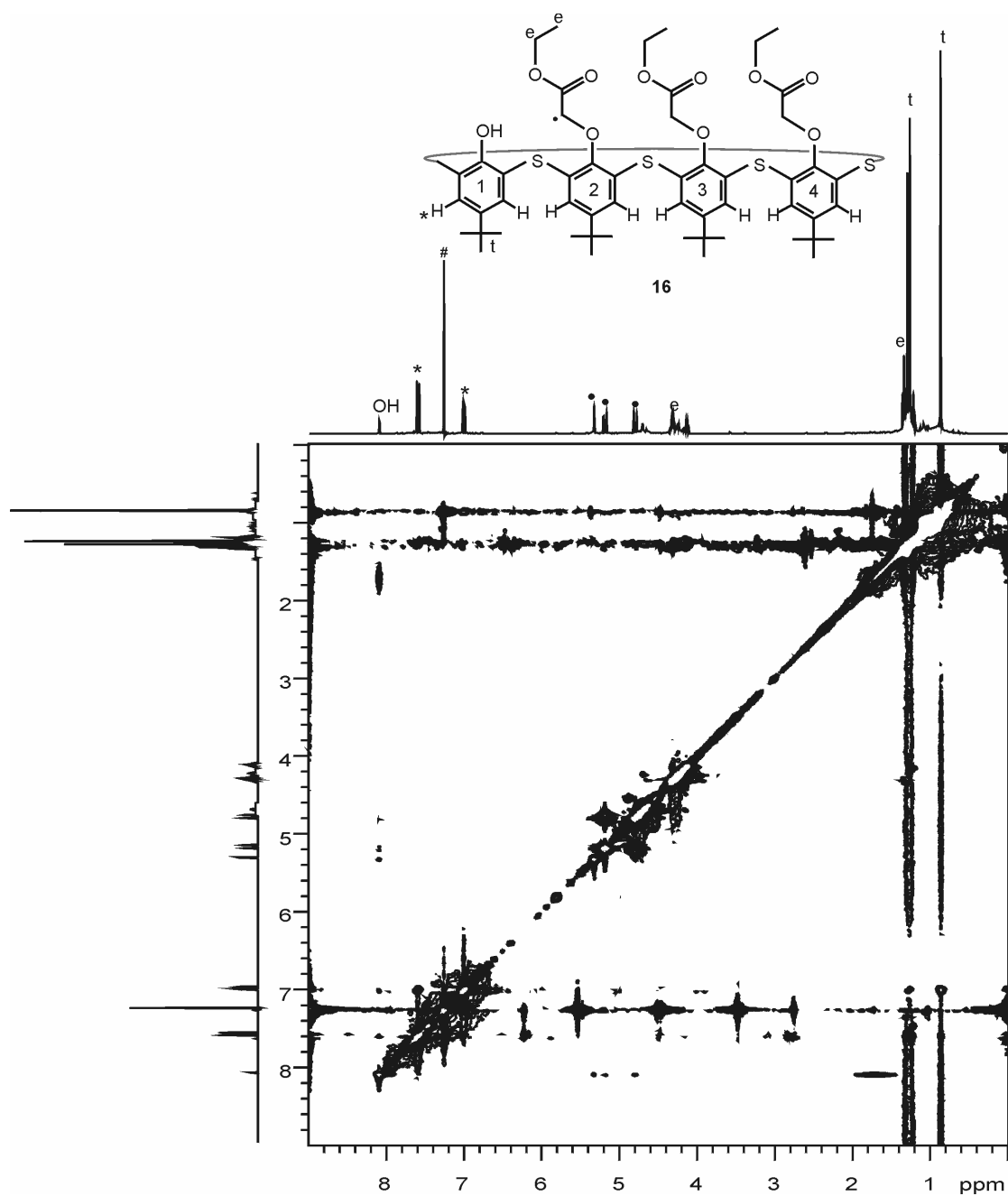
## 2D $^1\text{H}$ NMR Spectra



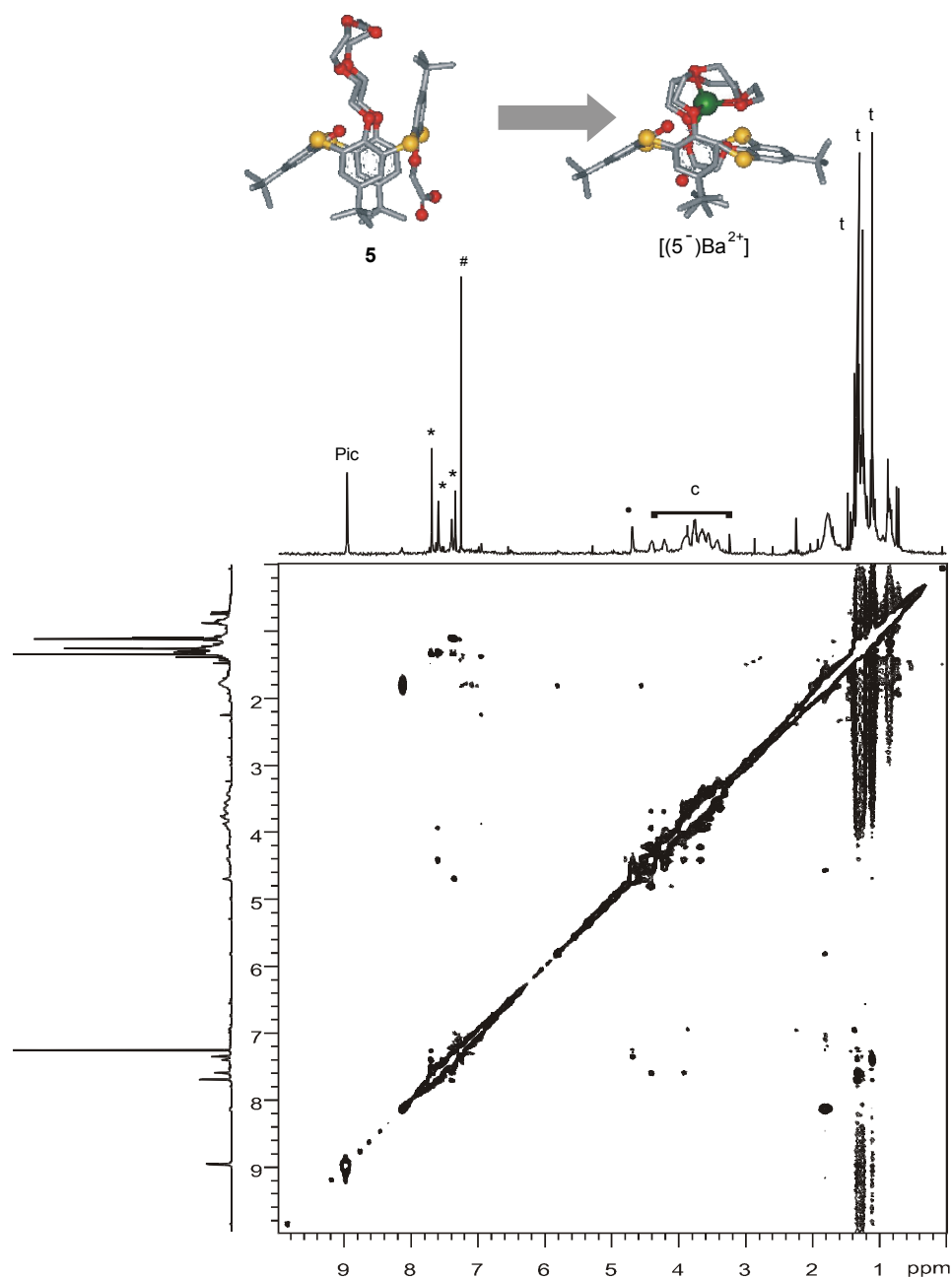
**Figure S1.** ROESY spectrum of the thiacalix[4]crown monocarboxylic acid (2) (cone) in  $\text{CDCl}_3$  at 25 °C. The  $\text{CHCl}_3$  peak is indicated with #.



**Figure S2.** NOESY spectrum of the thiacalix[4]crown monocarboxylic acid (7) (partial cone) in CDCl<sub>3</sub> at 25 °C. The CHCl<sub>3</sub> peak is indicated with #.



**Figure S3.** NOESY spectrum of the thiacalix[4]arene-crown tricarboxylic ethyl ester (**16**; cone) in CDCl<sub>3</sub> at 25 °C. The CHCl<sub>3</sub> peak is indicated with #.



**Figure S4.** NOESY spectrum of the thiacalix[4]crown monocarboxylic acids (**5**) (partial cone)  $\text{Ba}^{2+}$  complex in  $\text{CDCl}_3$  at 25 °C. Indicated are the resonances of: the  $-\text{OCH}_2\text{CO}_2^-$  group ( $^\circ$ ), the crown-ether bridge ( $^c$ ), the ArH groups ( $^*$ ), the *t*-butyl groups ( $^t$ ), and  $\text{CHCl}_3$  ( $^\#$ ). The expected conformational change of **5** (Figure S2) after complexation of  $\text{Ba}^{2+}$  is depicted as molecular model (top Figure S4).

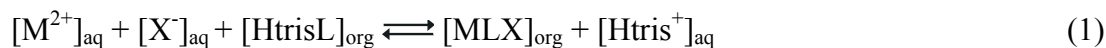
### Extraction equilibria and stoichiometries used to obtain extraction constants

Comparison of the extraction constants of the competing cations ( $\text{Ca}^{2+}$ ,  $\text{Sr}^{2+}$ , and  $\text{Ba}^{2+}$ ) and of  $^{226}\text{Ra}^{2+}$ , allows the quantification of the differences between the various extractants used (**2**, **3a,b**, **4a,b**, **5**, **6**, **7**, and **8**). In order to obtain these extraction constant ratios, several equilibria have to be considered.

Since the  $\text{pK}_a$  of tris is 8.1<sup>1</sup> and all the competition experiments were performed at pH 8.9 ( $[\text{tris}]_{\text{tot}} = 5.0 \times 10^{-2}$  M),  $[\text{Htris}^+]_{\text{aq}} = 6.8 \times 10^{-3}$  M. Consequently, because of the basic nature of the aqueous phase, the uncomplexed ligands ( $[\text{L}]_{\text{tot}} = 10^{-4}$  M) in the organic phase are assumed to exist as neutral  $(\text{Htris})\text{L}$ ,  $(\text{Htris})_2\text{L}$ ,  $(\text{Htris})_3\text{L}$ , or  $(\text{Htris})_4\text{L}$  salts, depending on the charge of the ligand.

#### *Singly Charged Extractants, 1: 1 Stoichiometry (2 and 5)*

Extraction of  $\text{M}^{2+}$  cations by the singly charged thiocalix[4]crown monocarboxylic acids (**2** and **5**) is shown in Figure S.5. The best fits were obtained assuming a 1:1 complex stoichiometry, and therefore the equilibrium for the extraction of the divalent cations can be written as equation 1, with equation 2 describing the corresponding extraction constant.



$$K_{\text{ex}}^{\text{M}} = \frac{[\text{MLX}]_{\text{org}}[\text{Htris}^+]_{\text{aq}}}{[\text{M}^{2+}]_{\text{aq}}[\text{HtrisL}]_{\text{org}}[\text{X}^-]_{\text{aq}}} \quad (2)$$

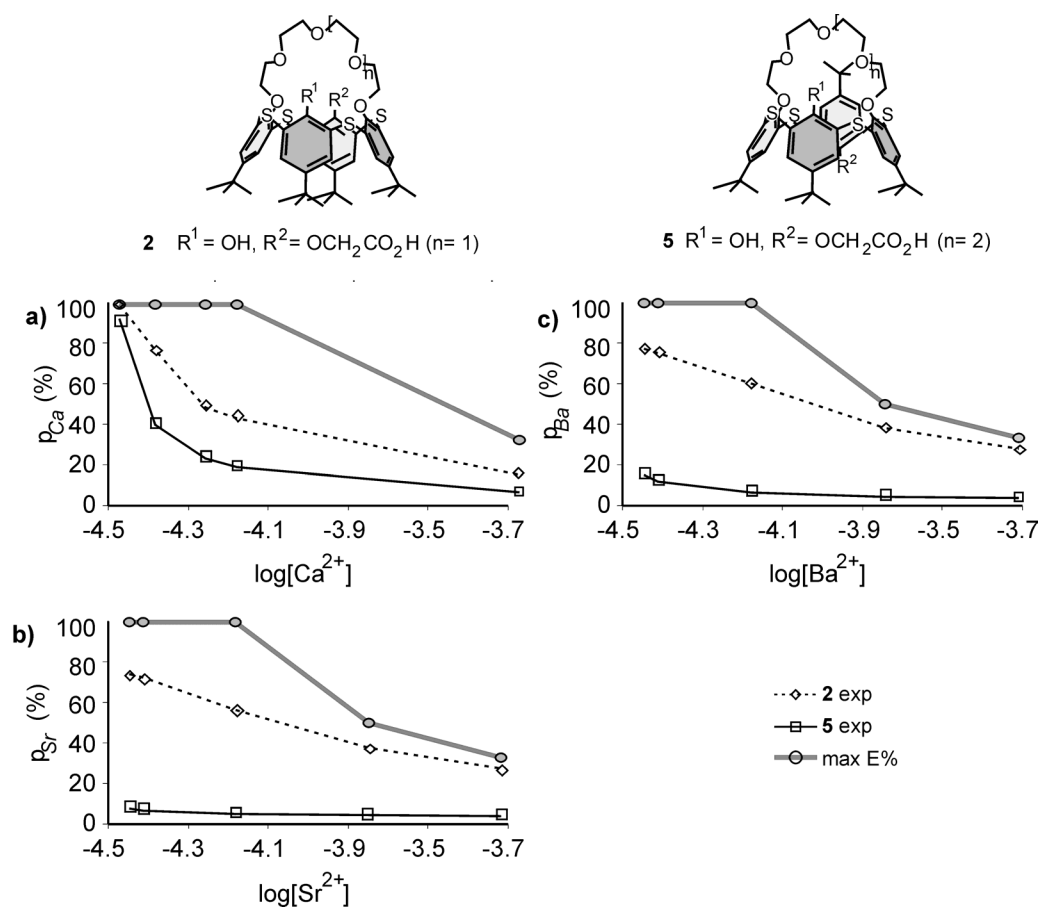
Because of the equal volumes used, a decrease of  $[\text{M}^{2+}]_{\text{aq}}$  in the aqueous phase leads to an equal increase of  $[\text{MLX}]_{\text{org}}$  in the organic phase, allowing for direct comparison of the concentrations of the two phases. This results in the equations 3 and 4 for the mass balances of  $\text{M}^{2+}$  and L, respectively.

$$[M^{2+}]_{\text{tot}} = [M^{2+}]_{\text{aq}} + [\text{MLX}]_{\text{org}} \quad (3)$$

$$[L]_{\text{tot}} = [(\text{Htris})_2L]_{\text{org}} + [\text{MLX}]_{\text{org}} \quad (4)$$

If the extraction percentages obtained for the competing cations (see Figure S.5) are incorporated as  $p_M = [\text{MLX}]_{\text{org}}/[M^{2+}]_{\text{tot}}$ ,  $[\text{MLX}]_{\text{org}}$  is equal to  $p_M[M^{2+}]_{\text{tot}}$ , and  $[M^{2+}]_{\text{aq}} = (1-p_M)[M^{2+}]_{\text{tot}}$ .

The extraction percentages of the competing  $M^{2+}$  cations in a concentration range of  $(0.2-3.0) \times 10^{-4} \text{ M}$  are provided in Figure S.5. From these extraction curves,  $K_{\text{ex}}^M$  can be obtained by fitting calculated  $p_M$  values to the experimentally determined values (Table 2), using a non-linear least squares fitting procedure.



**Figure S.5.**  $M^{2+}$  extraction percentages ( $p_M = [M^{2+}]_{\text{org}}/[M^{2+}]_{\text{tot}}(\%)$ ) for extractants **2** and **5** ( $10^{-4}$  M; 1 ml of  $\text{CH}_2\text{Cl}_2$ ) as a function of  $\log[M^{2+}]$  ( $M^{2+} = \text{Ca}^{2+}$ (a),  $\text{Sr}^{2+}$ (b), and  $\text{Ba}^{2+}$ (c); 1 ml of water pH 8.9 tris-HCl buffer). The line through the circles gives the extraction percentages calculated for the complex formation of a 1:1 [MLX] complex.

When the  $^{226}\text{Ra}^{2+}$  experiments, in competition with the divalent cations  $\text{Ca}^{2+}$ ,  $\text{Sr}^{2+}$ , and  $\text{Ba}^{2+}$  (Figure 3), are modelled, additional equilibria and mass balances have to be considered. The extraction equilibrium for  $^{226}\text{Ra}^{2+}$  and its extraction constant are given in equations 5 and 6, respectively. The  $^{226}\text{Ra}^{2+}$  mass balance is given in equation 7, and the ligand mass balance (equation 4) is now expanded to equation 8.



$$K_{\text{ex}}^{\text{Ra}} = \frac{[^{226}\text{RaLX}]_{\text{org}}[\text{Htris}^+]_{\text{aq}}}{[^{226}\text{Ra}^{2+}]_{\text{aq}}[\text{HtrisL}]_{\text{org}}[\text{X}^-]_{\text{aq}}} \quad (6)$$

$$[^{226}\text{Ra}^{2+}]_{\text{tot}} = [^{226}\text{Ra}^{2+}]_{\text{aq}} + [^{226}\text{RaLX}]_{\text{org}} \quad (7)$$

$$[\text{L}]_{\text{tot}} = [\text{HtrisL}]_{\text{org}} + [\text{MLX}]_{\text{org}} + [^{226}\text{RaLX}]_{\text{org}} \quad (8)$$

However, because of the small amount of  $[^{226}\text{Ra}^{2+}]_{\text{tot}}$  ( $2.9 \times 10^{-8}$  M),  $[^{226}\text{RaLX}]_{\text{org}}$  can be neglected in equation 8. Similar to  $p_M$  for the competing cations,  $p_{\text{Ra}}$  is defined as  $[^{226}\text{RaLX}]_{\text{org}}/[^{226}\text{Ra}^{2+}]_{\text{tot}}$ , resulting in  $[^{226}\text{RaLX}]_{\text{org}} = p_{\text{Ra}}[^{226}\text{Ra}^{2+}]_{\text{tot}}$ , and  $[^{226}\text{Ra}^{2+}]_{\text{aq}} = (1-p_{\text{Ra}})[^{226}\text{Ra}^{2+}]_{\text{tot}}$ . Thus the  $K_{\text{ex}}^{\text{Ra}}/K_{\text{ex}}^{\text{M}}$  ratio (equation 9) can be written as equation 10.

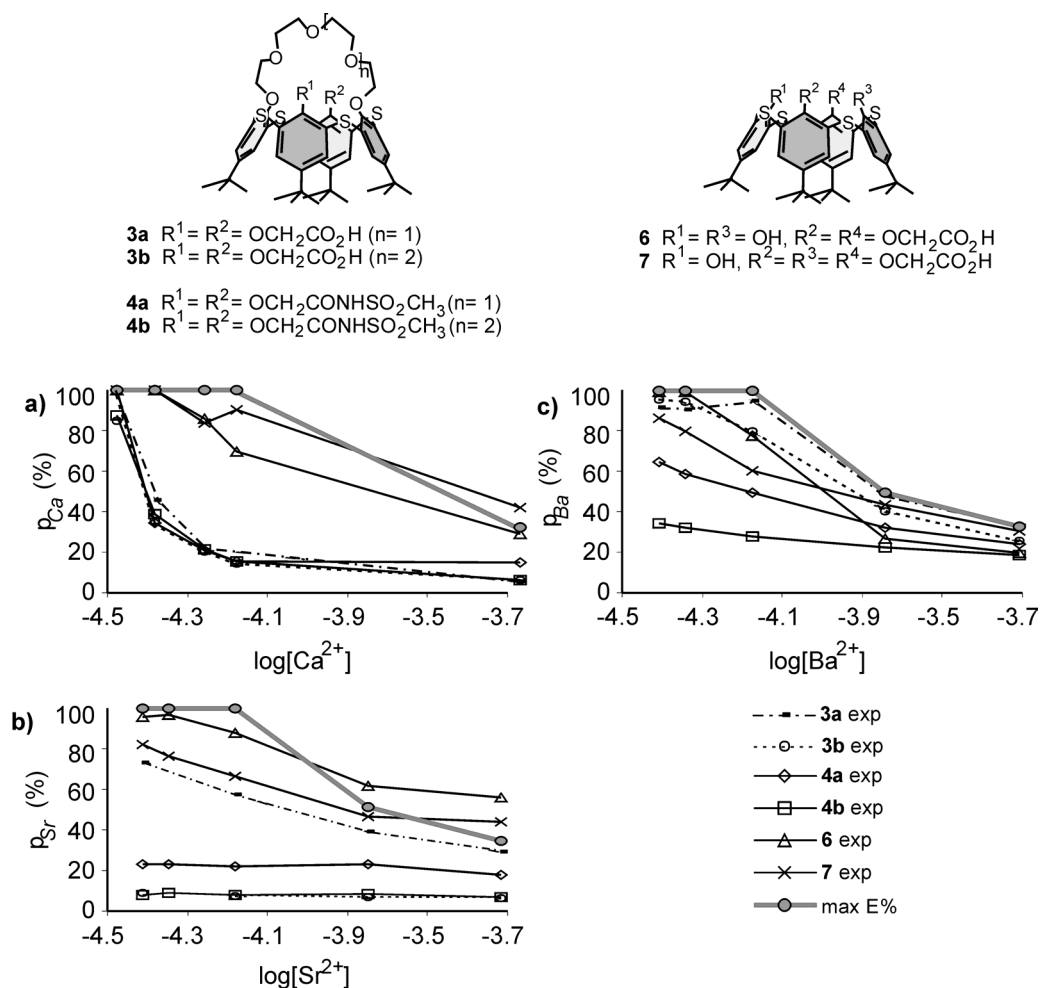
$$K_{\text{ex}}^{\text{Ra}}/K_{\text{ex}}^{\text{M}} = \frac{[^{226}\text{RaLX}]_{\text{org}}}{[^{226}\text{Ra}^{2+}]_{\text{aq}}} * \frac{[M^{2+}]_{\text{aq}}}{[\text{MLX}]_{\text{org}}} \quad (9)$$

$$K_{\text{ex}}^{\text{Ra}}/K_{\text{ex}}^{\text{M}} = p_{\text{Ra}}(1-p_M)/(1-p_{\text{Ra}})p_M \quad (10)$$



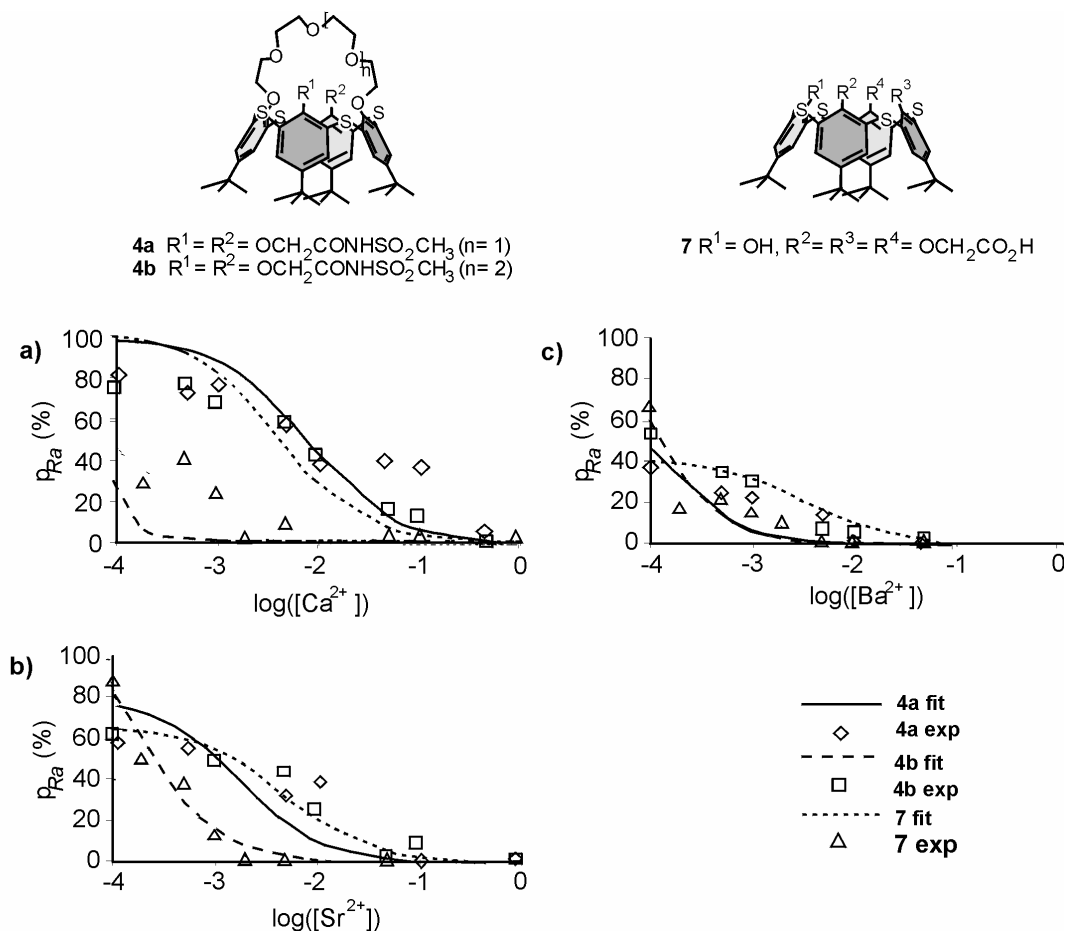
Since the  $K_{\text{ex}}^{\text{M}}$  values of the different extractants have different dimensions, only  $K_{\text{M}}^{\text{Ra}}/K_{\text{ex}}^{\text{M}}$  ratios are given. These ratios are obtained by fitting calculated  $p_{\text{Ra}}$  values to the experimentally determined values (Figure 3), using a non-linear least squares fitting procedure.

*Di- or Trivalently Charged Extractants, 1: 1 Stoichiometry (3a,b, 4a,b, 6, and 7)*



**Figure S.6.**  $\text{M}^{2+}$  extraction percentages ( $p_{\text{M}^{2+}} = [\text{M}^{2+}]_{\text{org}}/[\text{M}^{2+}]_{\text{tot}}$  (%)) for extractants **3a,b**, **4a,b**, **6**, and **7** ( $10^{-4}$  M; 1 ml of  $\text{CH}_2\text{Cl}_2$ ) as a function of  $\log[\text{M}^{2+}]$  ( $\text{M}^{2+} = \text{Ca}^{2+}$ (a),  $\text{Sr}^{2+}$ (b), and  $\text{Ba}^{2+}$ (c); 1 ml of water pH 8.9 tris-HCl buffer). The line

through the circles gives the extraction percentages calculated for a 1:1 [ML] complex.

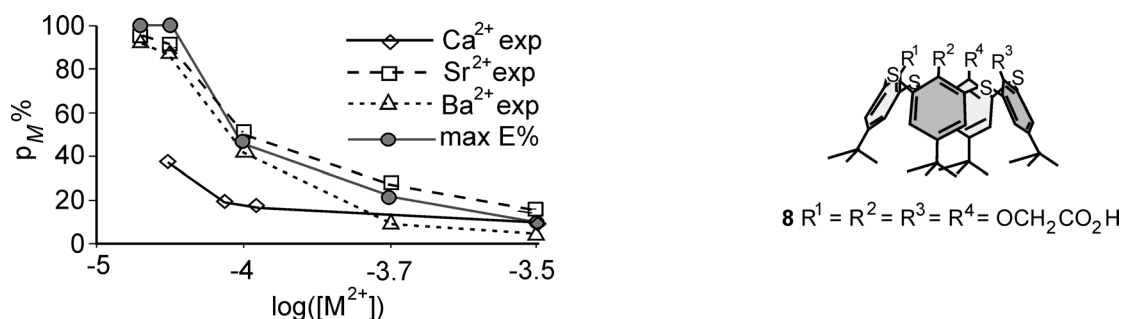


**Figure S.7.**  $^{226}\text{Ra}^{2+}$  extraction percentages ( $p_{\text{Ra}} = \frac{[^{226}\text{Ra}^{2+}]_{\text{org}}}{[^{226}\text{Ra}^{2+}]_{\text{tot}}} (\%)$ ) for extractants **4a** (a), **4b** (b), and **7** (c) ( $10^{-4}$  M; 1 ml of  $\text{CH}_2\text{Cl}_2$ ), as a function of the  $\text{M}(\text{NO}_3)$  ( $\text{M}^{2+} = \text{Ca}^{2+}$ ,  $\text{Sr}^{2+}$ , or  $\text{Ba}^{2+}$ ; 1 ml of water pH 8.9 tris-HCl buffer) concentration, with  $2.9 \times 10^{-8}$  M  $^{226}\text{Ra}^{2+}$ .

The equations used to determine the extraction constants and selectivity coefficient of the divalently charged thiacalix[4]crown dicarboxylic acids (**3a,b**) have previously been described.<sup>2</sup> For thiacalix[4]crown bis(methylsulfonyl) carboxamides

(4a,b), thiacalix[4]arene dicarboxylic acid (6), and thiacalix[4]arene tricarboxylic acid (7) the same equations can be used, which results in equation 10 for the  $^{226}\text{Ra}^{2+}$  selectivity coefficient. Here only the extraction behavior of 3a,b, 4a,b, 6, and 7 towards  $\text{Ca}^{2+}$ ,  $\text{Sr}^{2+}$ , and  $\text{Ba}^{2+}$  are depicted in Figure S.6, as well as the  $^{226}\text{Ra}^{2+}$  extraction curves of 4a,b and 7 (Figure S.7).

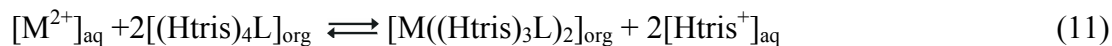
*Tetravalent Charged Extractant, 1: 2 Stoichiometry (8)*



**Figure S.8.**  $M^{2+}$  extraction percentages ( $p_M = [M^{2+}]_{\text{org}}/[M^{2+}]_{\text{tot}}$  (%)) recorded with **8** at different extractant to  $M(\text{NO}_3)_2$  ratios ( $M^{2+} = \text{Ca}^{2+}$ ,  $\text{Sr}^{2+}$ , and  $\text{Ba}^{2+}$ ; 1 ml of pH 8.9 tris-HCl buffer), using a fixed extractant ( $10^{-4}$  M; 1 ml of  $\text{CH}_2\text{Cl}_2$ ). The line through the circles gives the extraction percentages calculated for a 1:2  $[M(\text{Htris})_3\text{L}]_2$  complex stoichiometry.

Surprisingly, extraction data obtained for the thiacalix[4]arene tetracarboxylic acid (**8**), with the competing cations  $\text{Ca}^{2+}$ ,  $\text{Sr}^{2+}$ , and  $\text{Ba}^{2+}$  (Figure S.8) suggest a 1:2 ( $\text{ML}_2$ ) complex stoichiometry. Consequently, models based on a 1:2 stoichiometry could be used to fit these curves, while models based on more plausible 1:1 and 2:1 stoichiometries or a combination, did not give proper fits. As a result thereof, the

equilibrium for the extraction of the divalent cations can be written as equation 11, with equation 12 describing the corresponding extraction constant.



$$K_{\text{ex}}^M = [M((\text{Htris})_3\text{L})_2]_{\text{org}} [\text{Htris}^+]_{\text{aq}}^2 / [M^{2+}]_{\text{aq}} [(\text{Htris})_4\text{L}]_{\text{org}}^2 \quad (12)$$

Because of the equal volumes used, a decrease of  $[M^{2+}]_{\text{aq}}$  in the aqueous phase leads to an equal increase of  $[M((\text{Htris})_3\text{L})_2]_{\text{org}}$  in the organic phase, allowing for direct comparison of the concentrations of the two phases. This results in the equations 13 and 14 for the mass balances of  $M^{2+}$  and L, respectively.

$$[M^{2+}]_{\text{tot}} = [M^{2+}]_{\text{aq}} + [M((\text{Htris})_3\text{L})_2]_{\text{org}} \quad (13)$$

$$[L]_{\text{tot}} = [(\text{Htris})_4\text{L}]_{\text{org}} + 2[M((\text{Htris})_3\text{L})_2]_{\text{org}} \quad (14)$$

The extraction percentages obtained for the competing cations (see Table 1) are incorporated in equations 12-14 as  $p_M = [M((\text{Htris})_3\text{L})_2]_{\text{org}} / [M^{2+}]_{\text{tot}}$ ,  $[M((\text{Htris})_3\text{L})_2]_{\text{org}} = p_M [M^{2+}]_{\text{tot}}$ , and  $[M^{2+}]_{\text{aq}} = (1-p_M)[M^{2+}]_{\text{tot}}$ .

The extraction percentages of the competing  $M^{2+}$  cations in a concentration range of  $(0.2-3.0) \times 10^{-4}$  M are provided in Figure S.8. From these extraction curves,  $K_{\text{ex}}^M$  can be obtained by fitting calculated  $p_M$  values to the experimentally determined values (Table 2), using a non-linear least squares fitting procedure.

When the  $^{226}\text{Ra}^{2+}$  experiments, in competition with the divalent cations  $\text{Ca}^{2+}$ ,  $\text{Sr}^{2+}$ , and  $\text{Ba}^{2+}$  (Figure S.9), are modelled, additional equilibria and mass balances have to be considered. The extraction equilibrium and its extraction constant are given

in equations 15 and 16, respectively. The  $^{226}\text{Ra}^{2+}$  mass balance is given in equation 17, and the ligand mass balance (equation 4) is now expanded to equation 18.



$$K_{\text{ex}}^{\text{Ra}} = \frac{[^{226}\text{Ra}((\text{Htris})_3\text{L})_2]_{\text{org}}[\text{Htris}^+]_{\text{aq}}^2}{[^{226}\text{Ra}^{2+}]_{\text{aq}}[(\text{Htris})_4\text{L}]_{\text{org}}^2} \quad (16)$$

$$[^{226}\text{Ra}^{2+}]_{\text{tot}} = [^{226}\text{Ra}^{2+}]_{\text{aq}} + [^{226}\text{Ra}((\text{Htris})_3\text{L})_2]_{\text{org}} \quad (17)$$

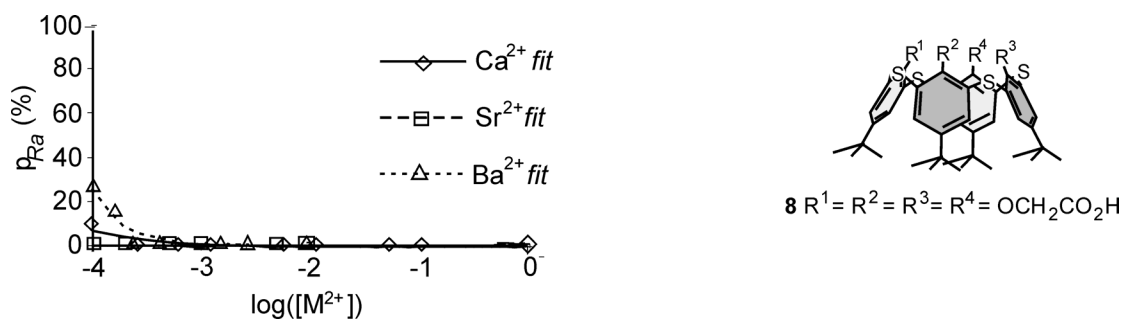
$$[\text{L}]_{\text{tot}} = [(\text{Htris})_4\text{L}]_{\text{org}} + 2[\text{M}((\text{Htris})_3\text{L})_2]_{\text{org}} + 2[^{226}\text{Ra}((\text{Htris})_3\text{L})_2]_{\text{org}} \quad (18)$$

However, because of the small amount of  $[^{226}\text{Ra}^{2+}]_{\text{tot}}$  ( $2.9 \times 10^{-8}$  M),  $[^{226}\text{Ra}((\text{Htris})_3\text{L})_2]_{\text{org}}$  can be neglected in equation 18. Similar to  $p_M$  for the competing cations,  $p_{Ra}$  is defined as  $[^{226}\text{Ra}((\text{Htris})_3\text{L})_2]_{\text{org}}/[^{226}\text{Ra}^{2+}]_{\text{tot}}$ , resulting in  $[^{226}\text{Ra}((\text{Htris})_3\text{L})_2]_{\text{org}} = p_{Ra}[^{226}\text{Ra}^{2+}]_{\text{tot}}$ , and  $[^{226}\text{Ra}^{2+}]_{\text{aq}} = (1-p_{Ra})[^{226}\text{Ra}^{2+}]_{\text{tot}}$ . Thus the  $K_{\text{ex}}^{\text{Ra}}/K_{\text{ex}}^{\text{M}}$  ratio (equation 19) can be written as equation 20.

$$K_{\text{ex}}^{\text{Ra}}/K_{\text{ex}}^{\text{M}} = \left( \frac{[^{226}\text{Ra}((\text{Htris})_3\text{L})_2]_{\text{org}}}{[^{226}\text{Ra}^{2+}]_{\text{aq}}} \right) * \left( \frac{[\text{M}^{2+}]_{\text{aq}}}{[\text{M}((\text{Htris})_3\text{L})_2]_{\text{org}}} \right) \quad (19)$$

$$K_{\text{ex}}^{\text{Ra}}/K_{\text{ex}}^{\text{M}} = p_{Ra}(1-p_M)/(1-p_{Ra})p_M \quad (20)$$

Since the  $K_{\text{ex}}^{\text{M}}$  values of the different extractants have different dimensions, only  $K_{\text{M}}^{\text{Ra}}/K_{\text{ex}}^{\text{M}}$  ratios are given. These ratios are obtained by fitting calculated  $p_{Ra}$  values to the experimentally determined values (Figure S.9), using a non-linear least squares fitting procedure.



**Figure S.9.**  $^{226}\text{Ra}^{2+}$  extraction percentages ( $p_{\text{Ra}} = [\text{Ra}^{2+}]_{\text{org}}/[\text{Ra}^{2+}]_{\text{tot}}$  (%)) for extractant **8** ( $10^{-4}$  M; 1 ml of  $\text{CH}_2\text{Cl}_2$ ), as a function of the  $\text{M}(\text{NO}_3)$  ( $\text{M} = \text{Ca}^{2+}$ ,  $\text{Sr}^{2+}$ , or  $\text{Ba}^{2+}$ ; 1 ml of water pH8.9 tris-HCl buffer) concentration, with  $2.9 \times 10^{-8}$  M  $^{226}\text{Ra}^{2+}$ . The fitted curves are depicted.

## References

1. Kearns, A.; Cole, L.; Haws, C. R.; Evans, D. E. *Plant Physiol. Biochem.* **1998**, *36*, 879-887.
2. Van Leeuwen, F. W. B.; Beijleveld, H.; Miermans, C. J. H.; Huskens, J.; Verboom, W.; Reinhoudt, D. N. *submitted for publication*.